

# Development of efficient *Escherichia coli* succinate production strains

**Ka-Yiu San**

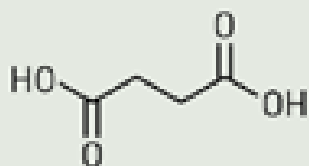
**Department of Bioengineering  
Department of Chemical and Biomolecular Engineering  
Rice University, Houston, Texas**

**International Conference  
Renewable Resources and Biorefineries  
Ghent – Belgium  
September, 20, 2005**

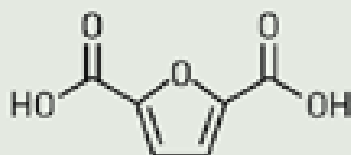


## BUILDING BLOCKS

DOE's Biomass Program identified 12 chemicals that can be produced from plant sugars and serve as key feedstocks in future biorefineries



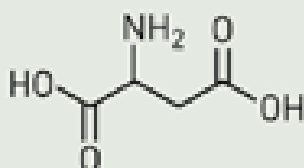
**Succinic acid<sup>a</sup>**



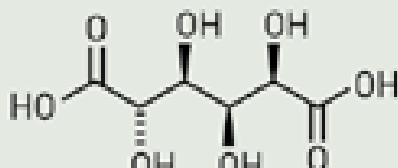
**2,5-Furandicarboxylic acid**



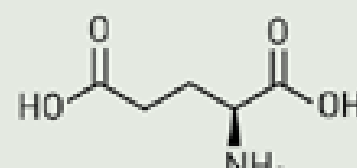
**3-Hydroxypropionic acid**



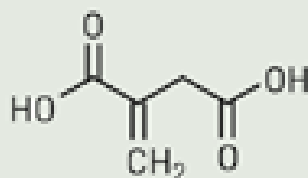
**Aspartic acid**



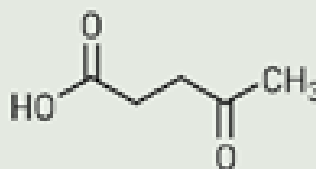
**Glucaric acid**



**Glutamic acid**



**Itaconic acid**



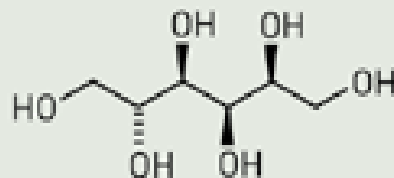
**Levulinic acid**



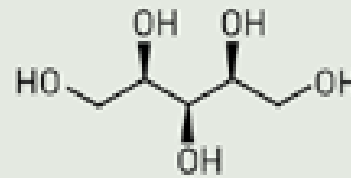
**3-Hydroxybutyrolactone**



**Glycerol**



**Sorbitol**



**Xylitol<sup>b</sup>**

**a** Class of 1,4-diacids also includes fumaric and malic acids. **b** Class of sugar alcohols also includes arabinitol.

Top Value Added Chemicals from Biomass (2004 DOE report)

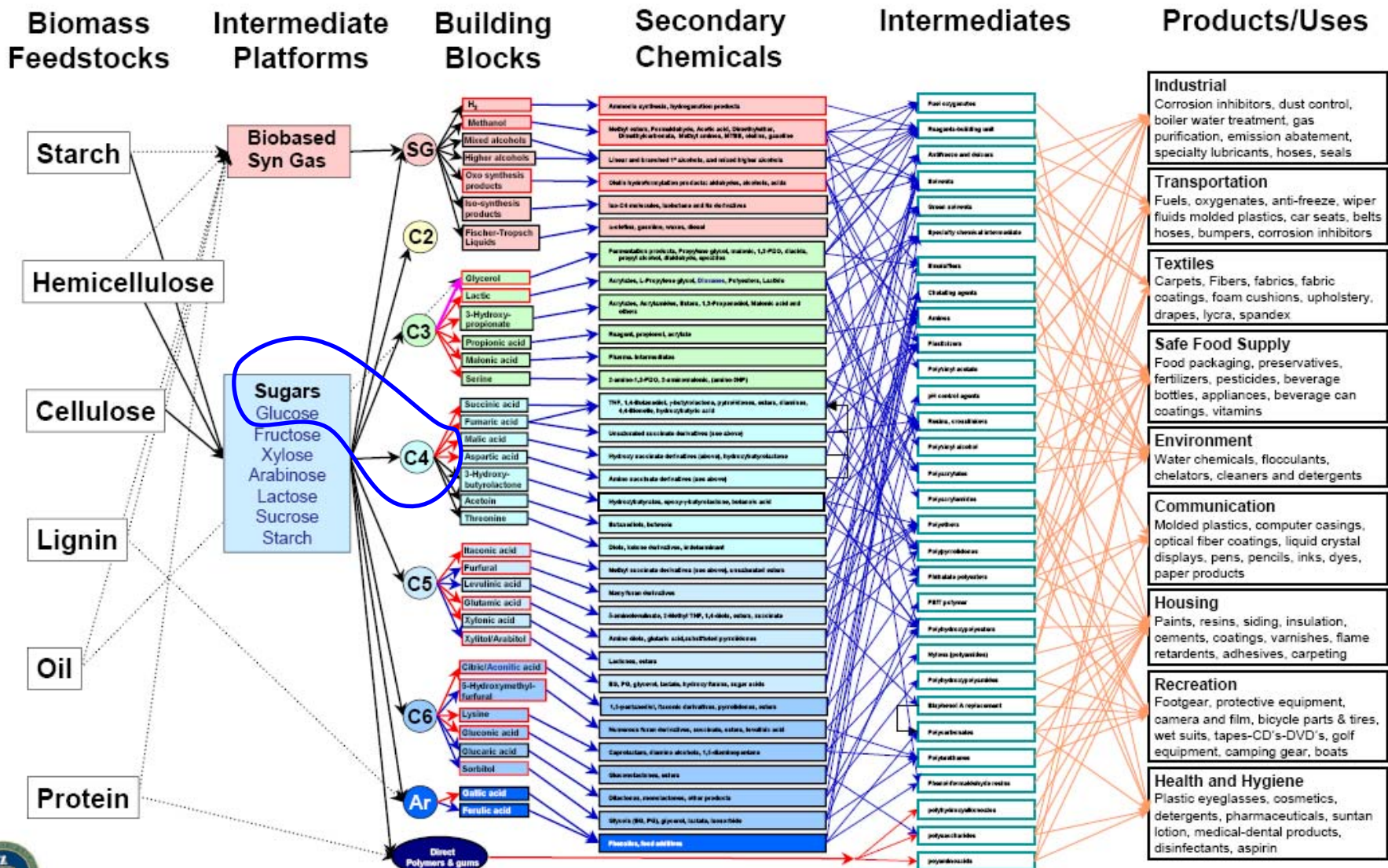
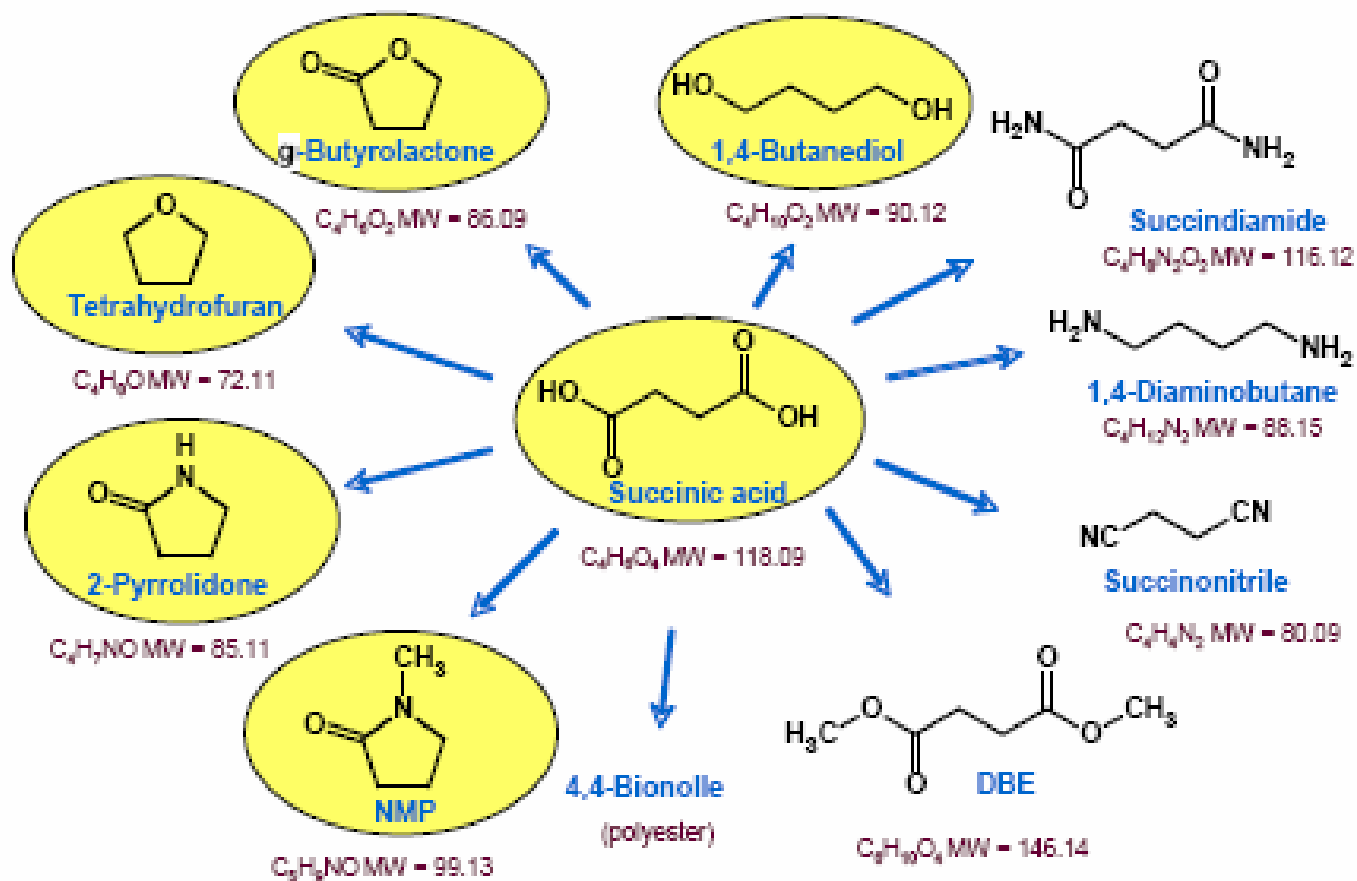


Figure 3 – Analogous Model of a Biobased Product Flow-chart for Biomass Feedstocks

Top Value Added Chemicals from Biomass (2004 DOE report)



*Succinic Acid Chemistry to Derivatives*

Top Value Added Chemicals from Biomass (2004 DOE report )

# Production of succinic acid

## Non-recombinant microorganisms :

- *A. succiniproducens*
- *A. succinogenes*
- *E. coli*
  - succinic acid minor fermentation product (~7.8% of total)

## Metabolically Engineered *E. coli*:

- Deletion of *ldh*
- overexpression of PEPC/ malic enzyme or PYC
- Deletion of *ldh* and *pfl*
  - NZN111
- Deletion of *ldh/pfl/ptsG*
  - APF111

# Current challenges

- ❖ **Existing strains have low productivity**
  - Low yield
  - Low production rate (weak strain)
- ❖ **Existing strains produce succinate anaerobically**
  - **need two stage fermentation**
- ❖ **Product purity – mixed acids fermentation**

# High yield anaerobic succinic acid production system

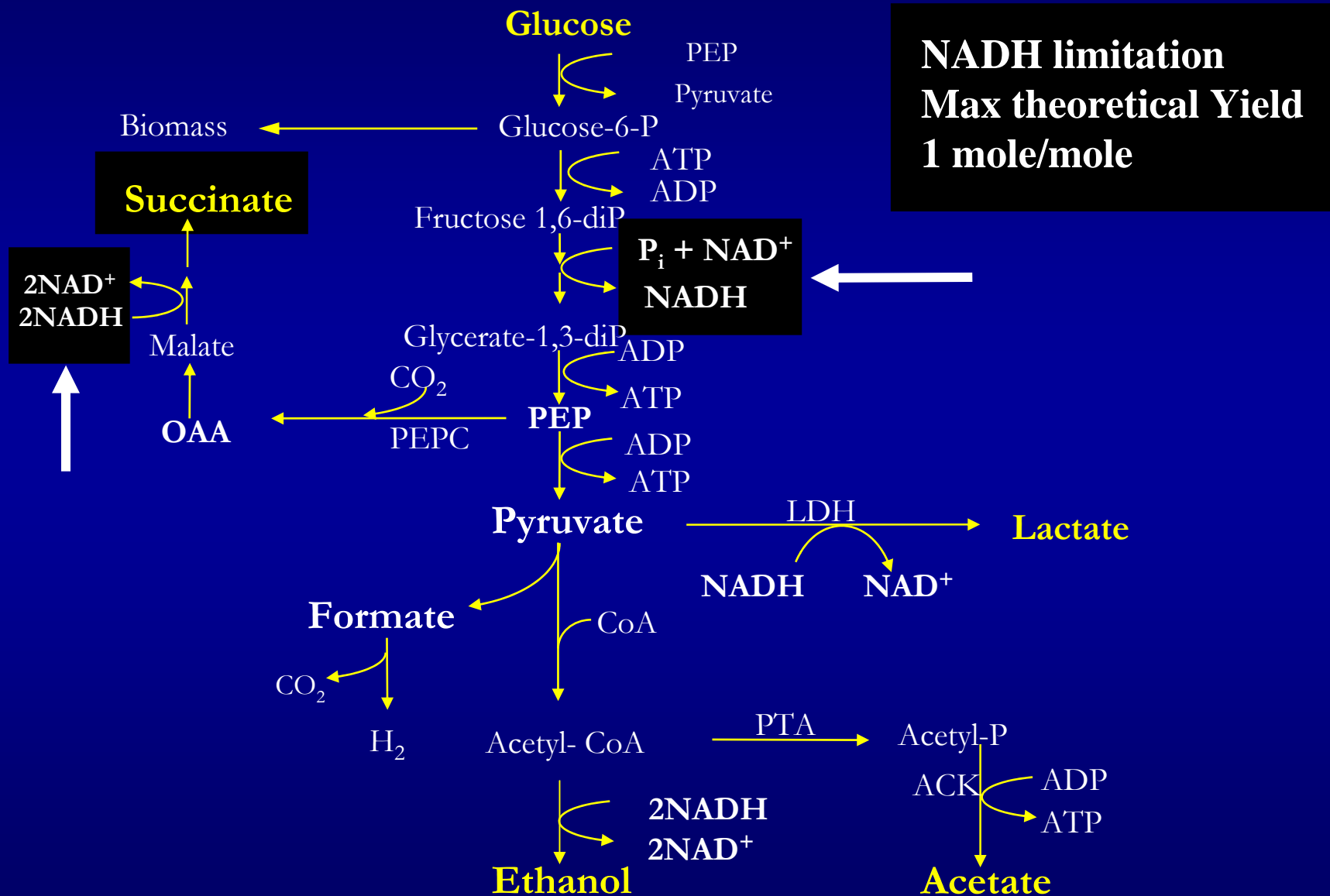
Design rationale...

High yield anaerobic succinic  
acid production system

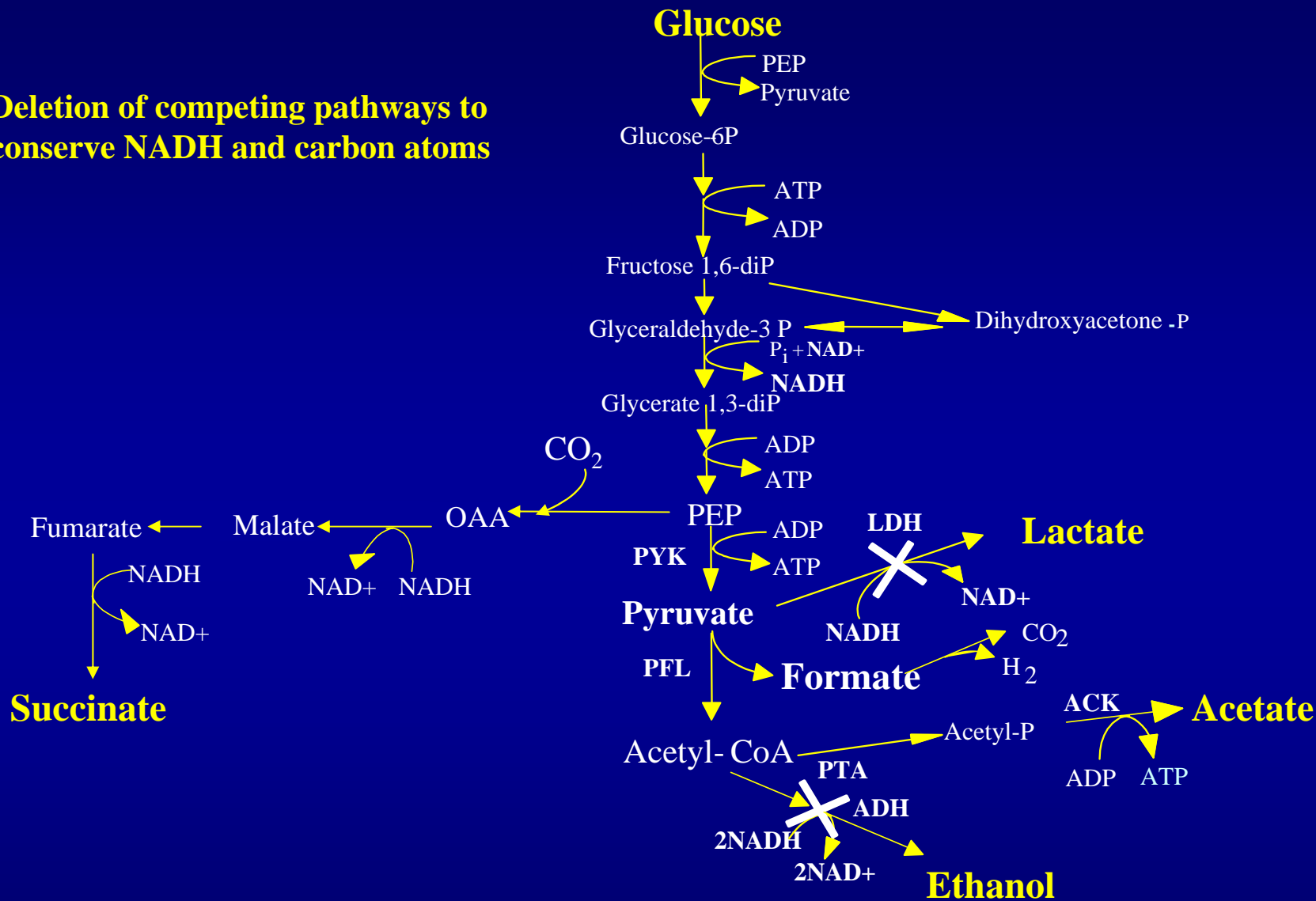
Limitation...



# Central anaerobic pathway in *E. coli*

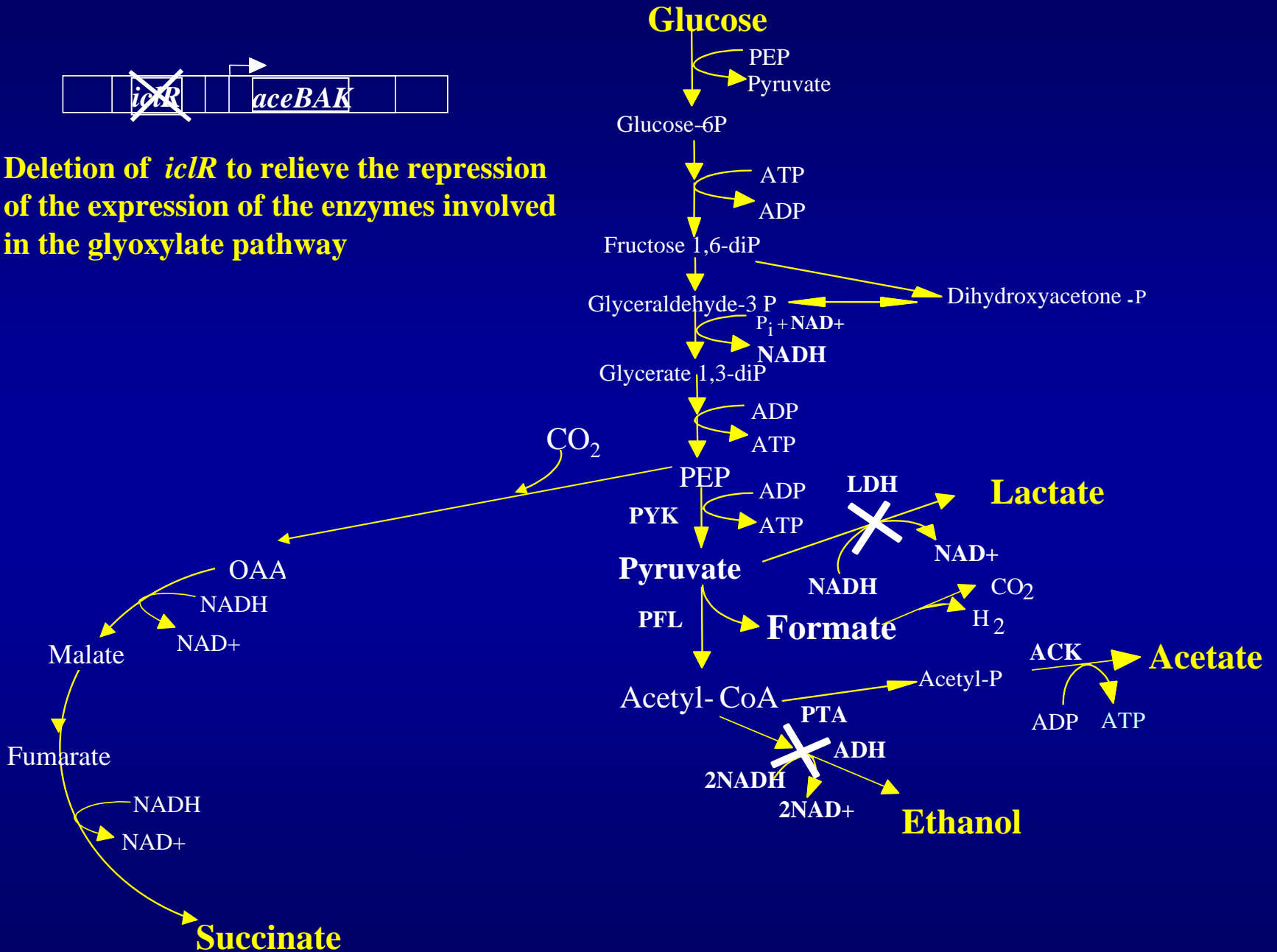


**1. Deletion of competing pathways to conserve NADH and carbon atoms**





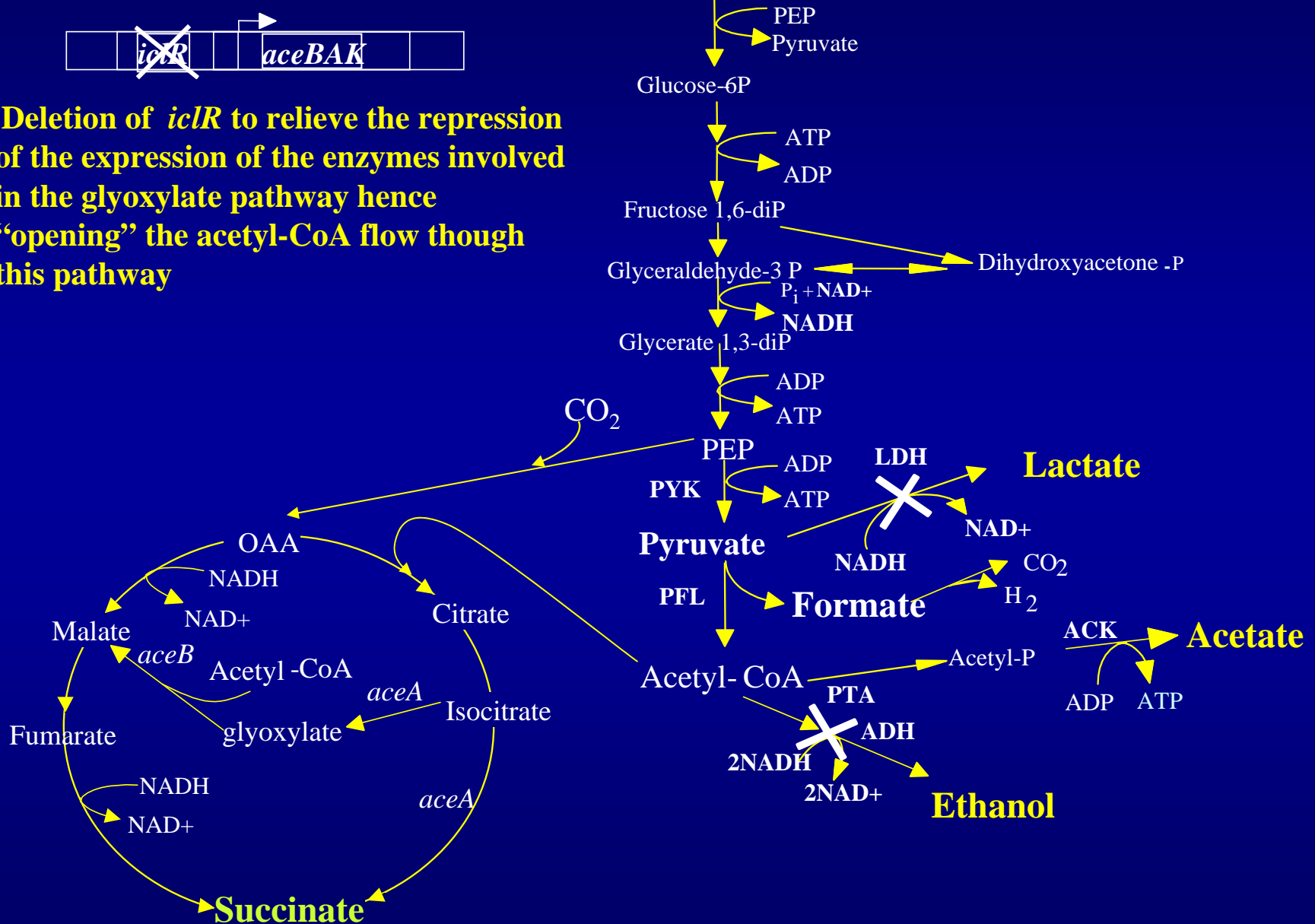
**2. Deletion of *iclR* to relieve the repression of the expression of the enzymes involved in the glyoxylate pathway**





2. Deletion of *iclR* to relieve the repression of the expression of the enzymes involved in the glyoxylate pathway hence “opening” the acetyl-CoA flow through this pathway

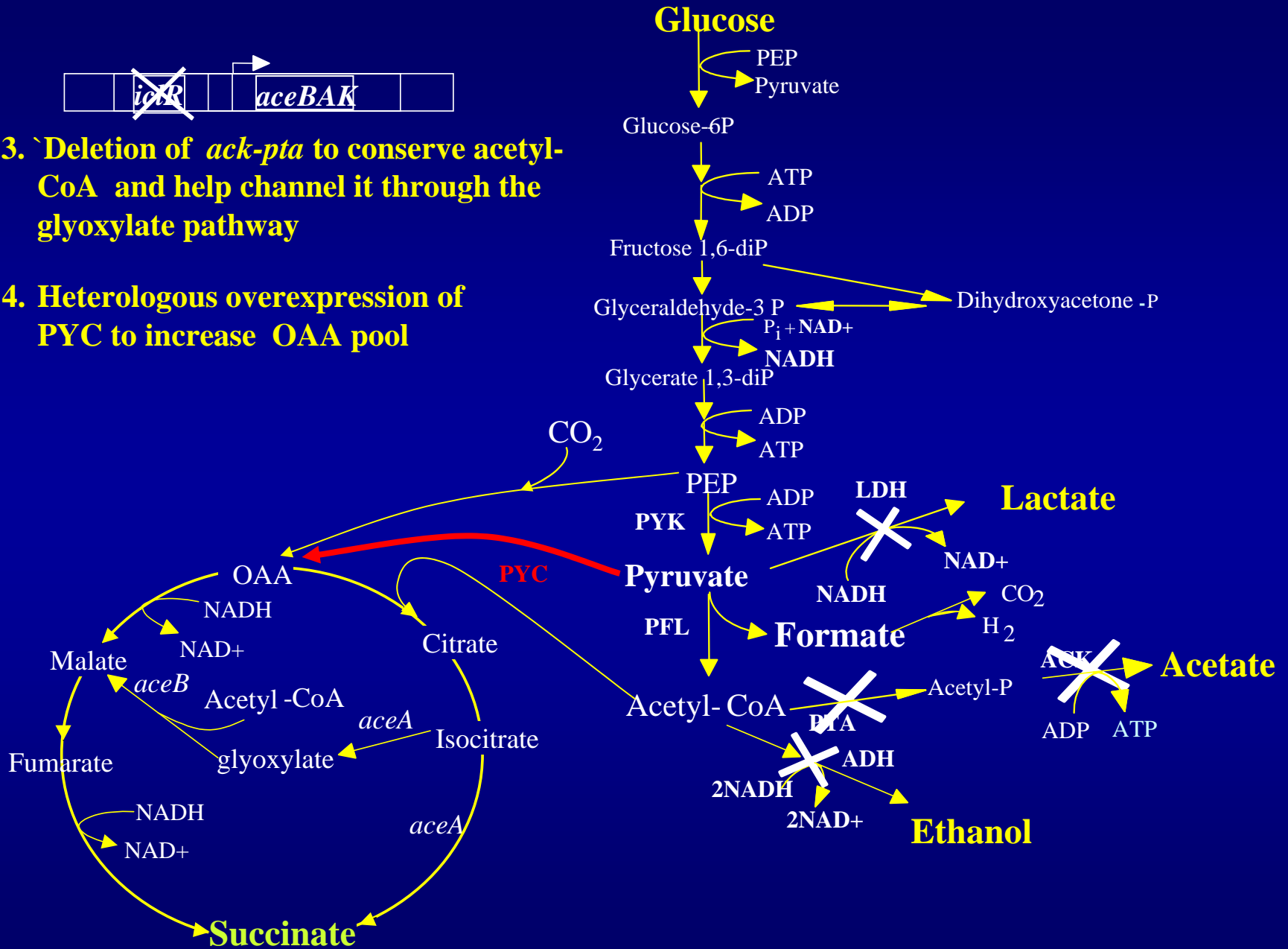
## Glucose





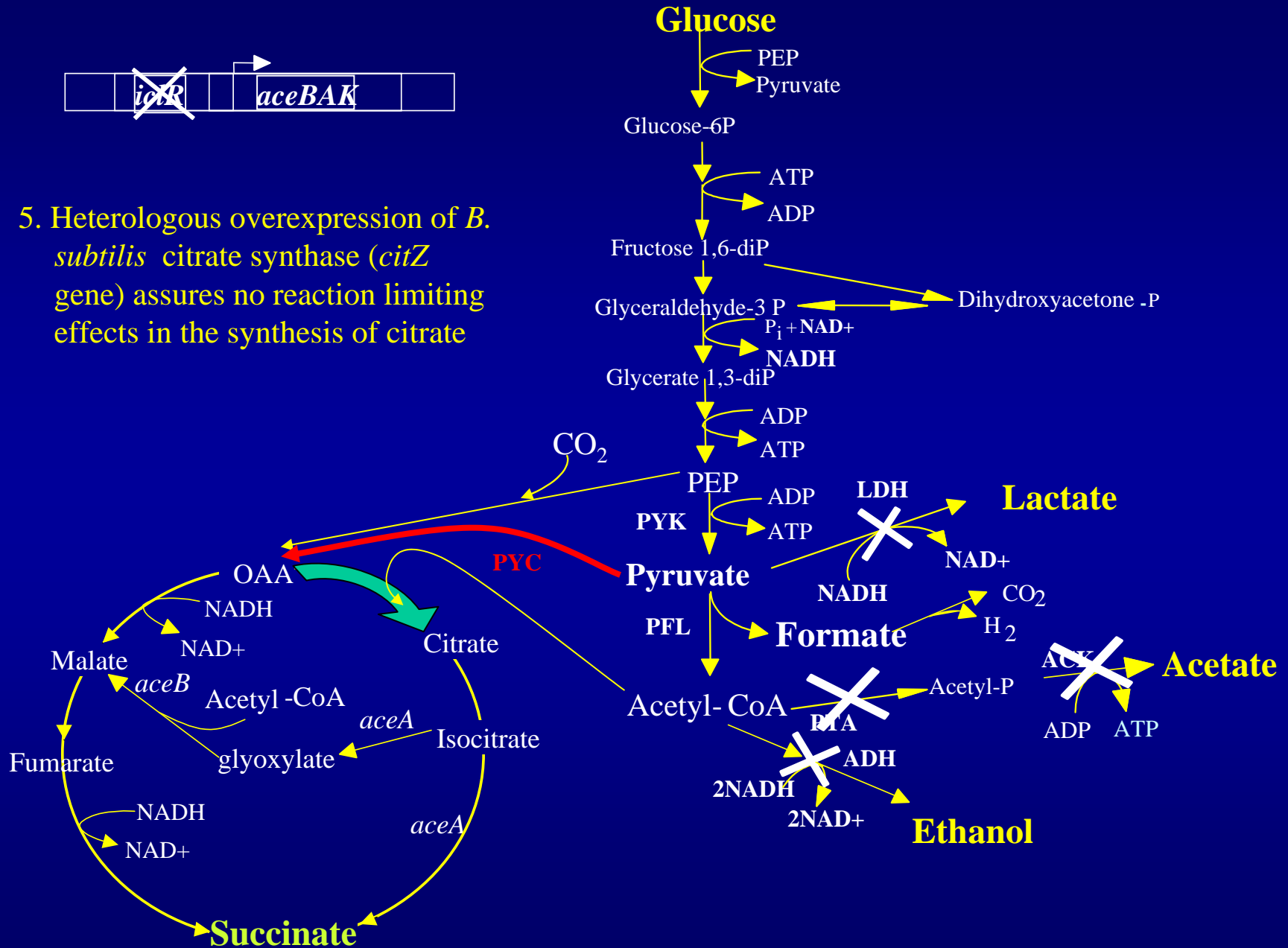
3. Deletion of *ack-pta* to conserve acetyl-CoA and help channel it through the glyoxylate pathway

4. Heterologous overexpression of *PYC* to increase OAA pool

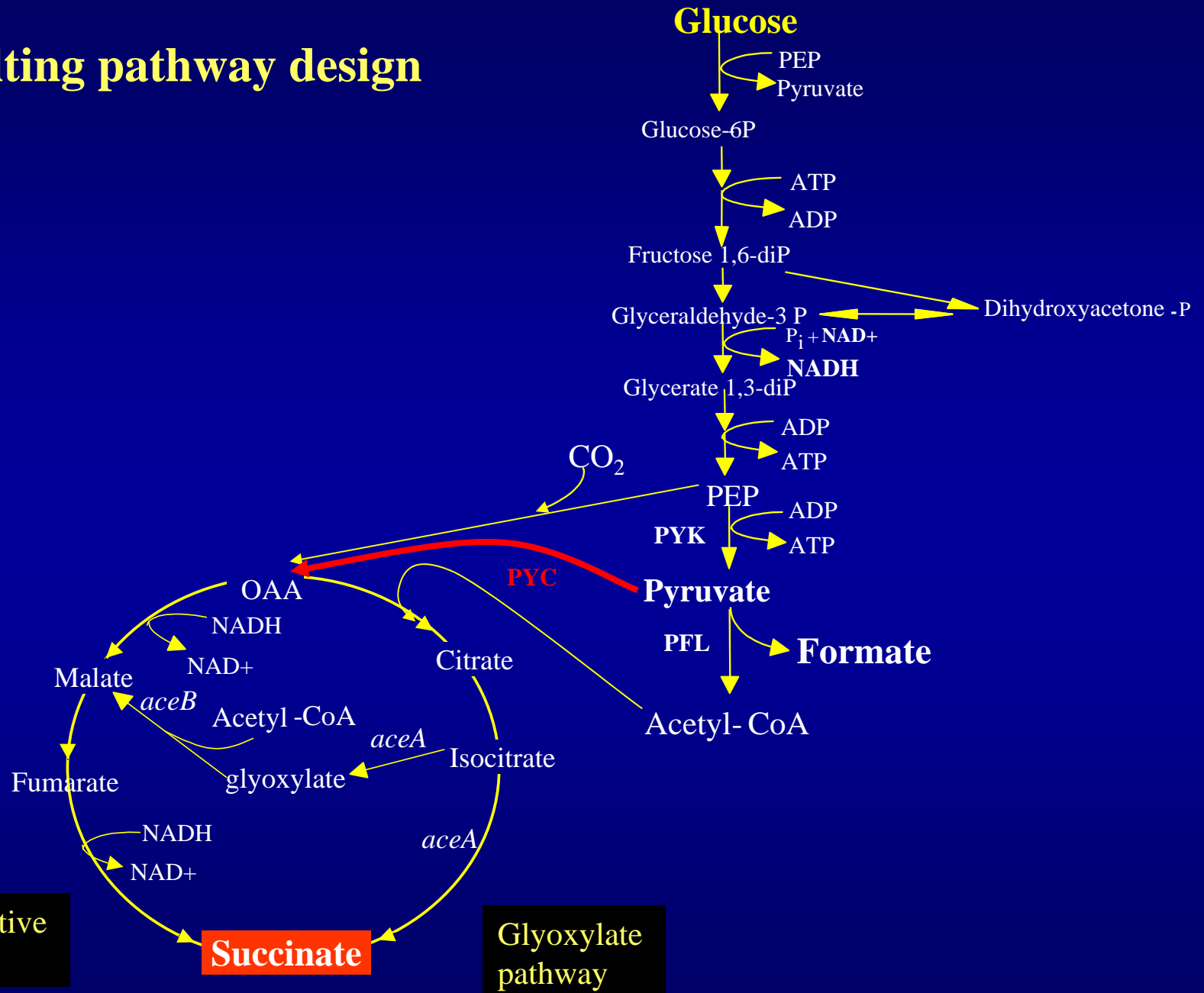




5. Heterologous overexpression of *B. subtilis* citrate synthase (*citZ* gene) assures no reaction limiting effects in the synthesis of citrate



# Resulting pathway design



# Experimental results

Strain SBS550MG

( $\Delta adhE \Delta ldhA \Delta iclR \Delta ackpta :: Cm^R$ )

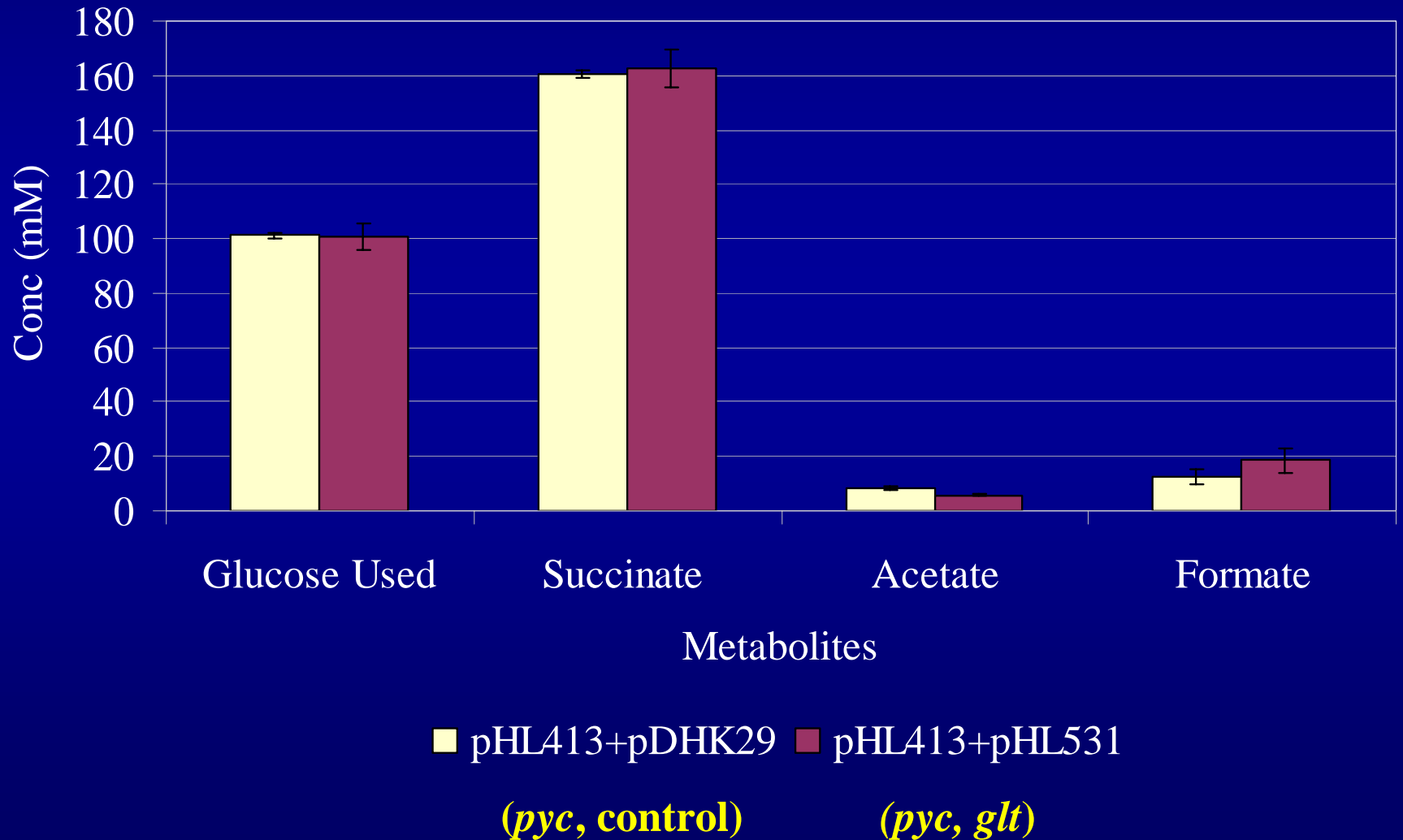
pHL413 - PYC, Ap<sup>R</sup>

pHL531 - Citrate Synthase, Km<sup>R</sup>

Fermentation Time: 24 hours

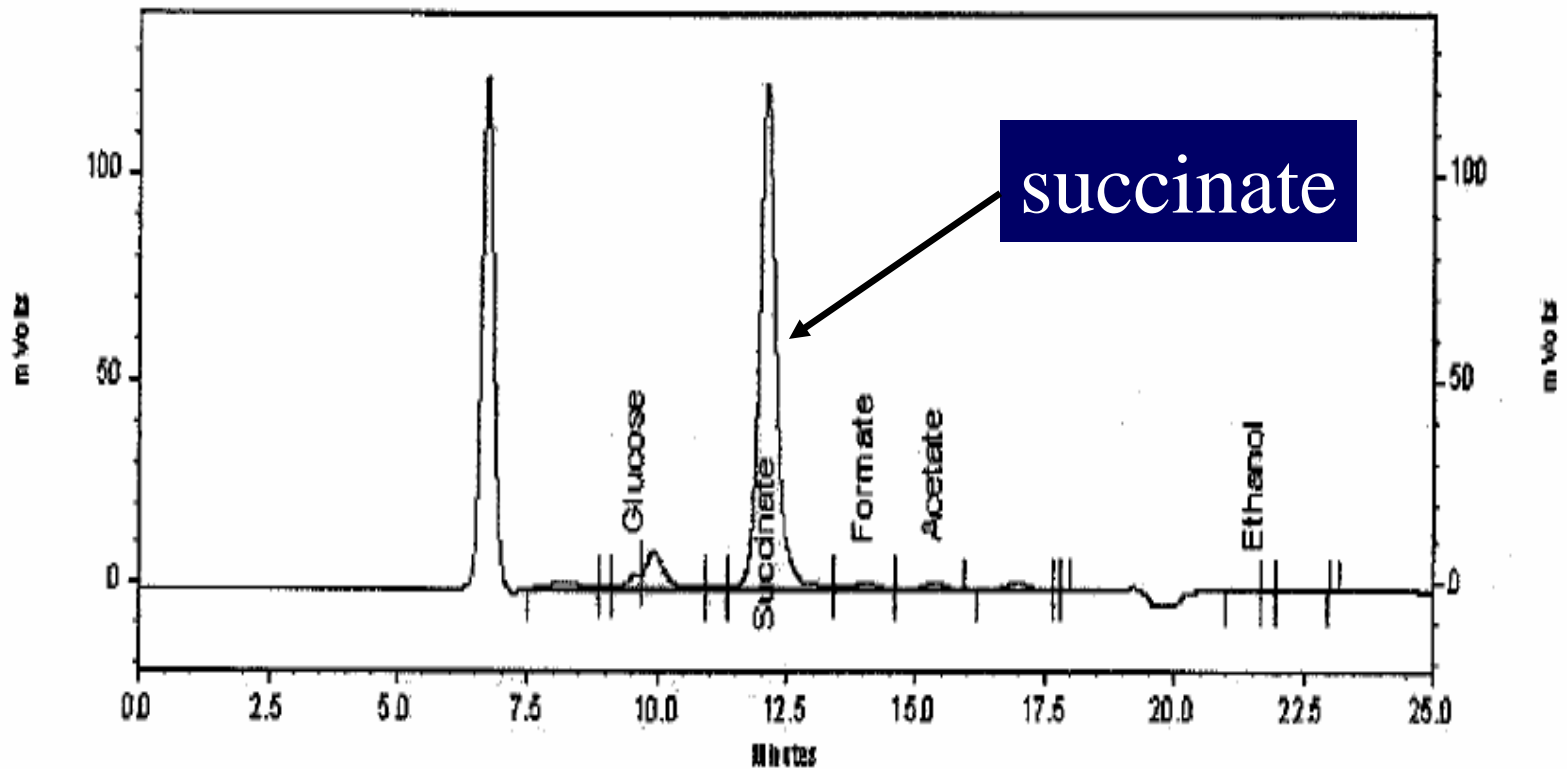


Strain SBS550MG  
( $\Delta adhE \Delta ldhA \Delta iclR \Delta ackpta :: Cm^R$ )

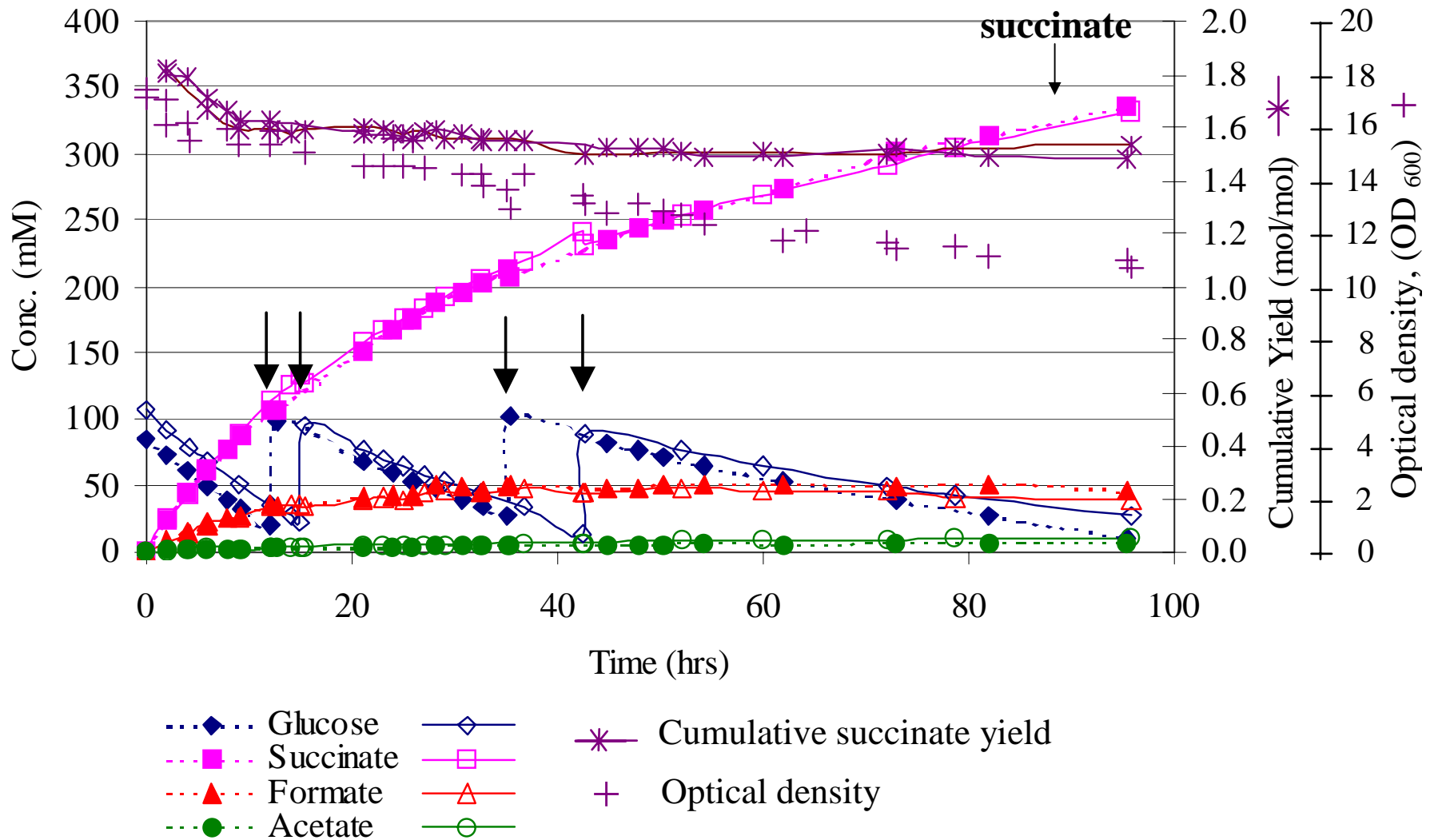


# Typical HPLC metabolite output

Sample name: SBS550MG (pHL413)

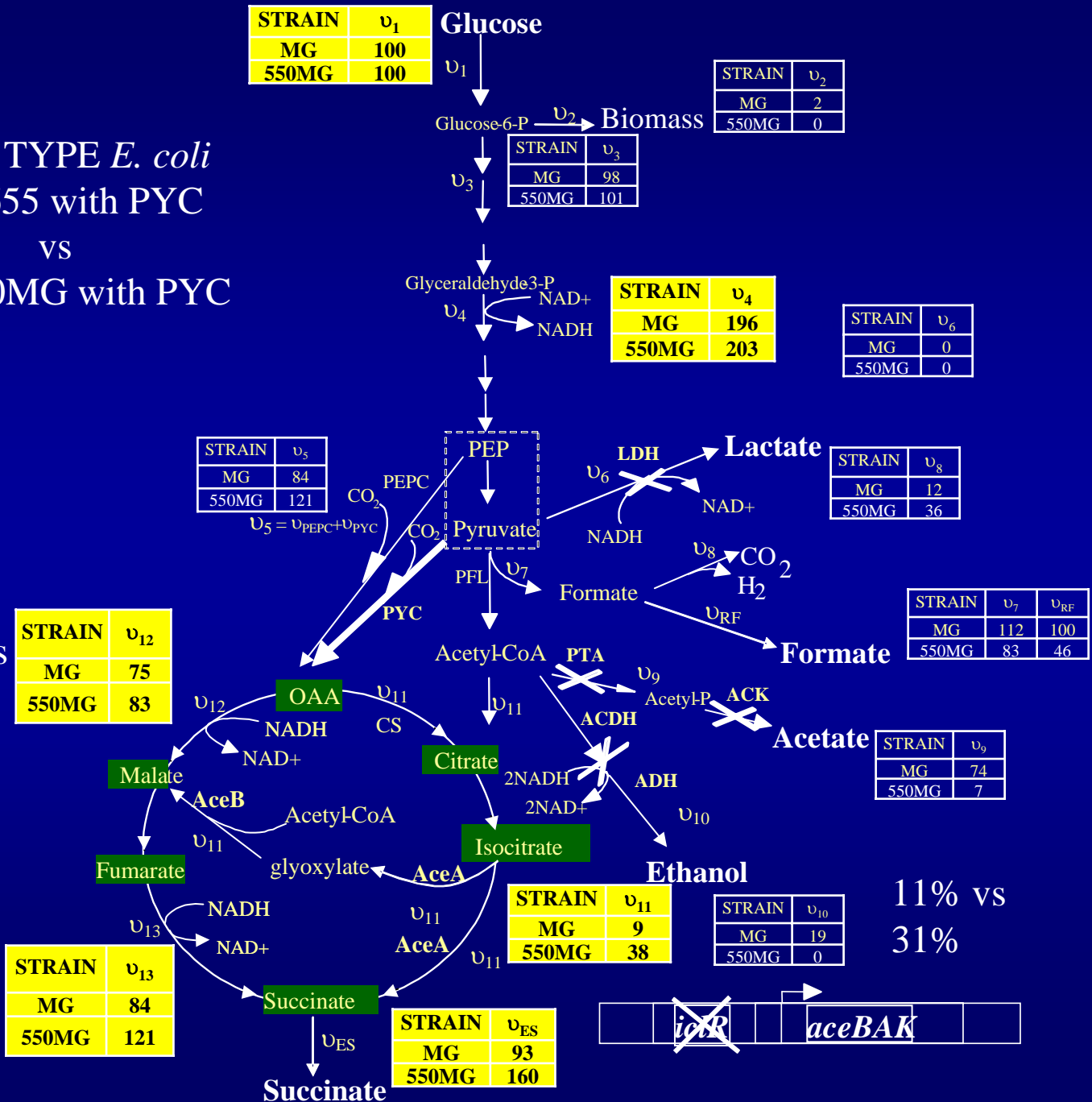


# Max usage of biocatalyst - Repeated feeding experiments

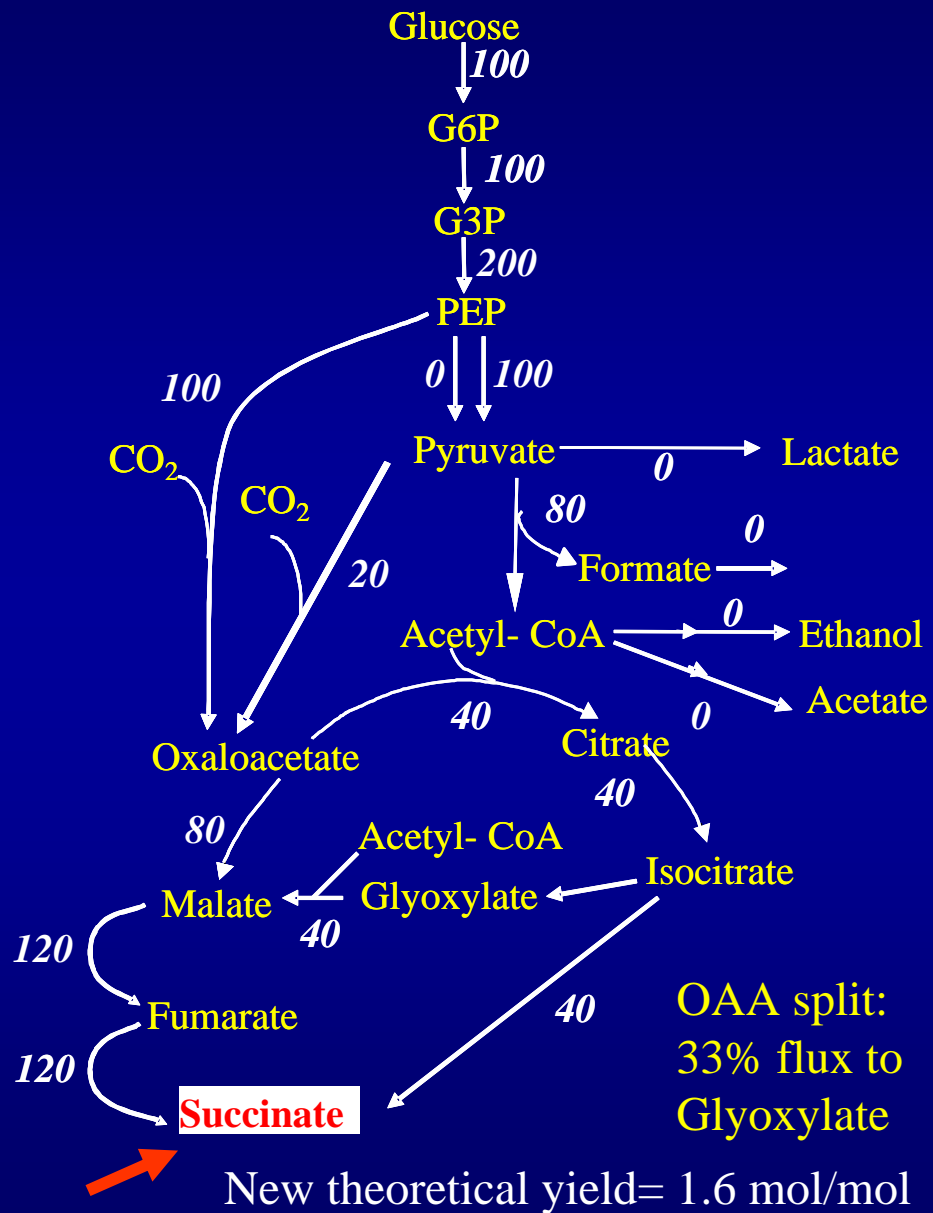


WILD TYPE *E. coli*  
MG1655 with PYC  
VS  
SBS550MG with PYC

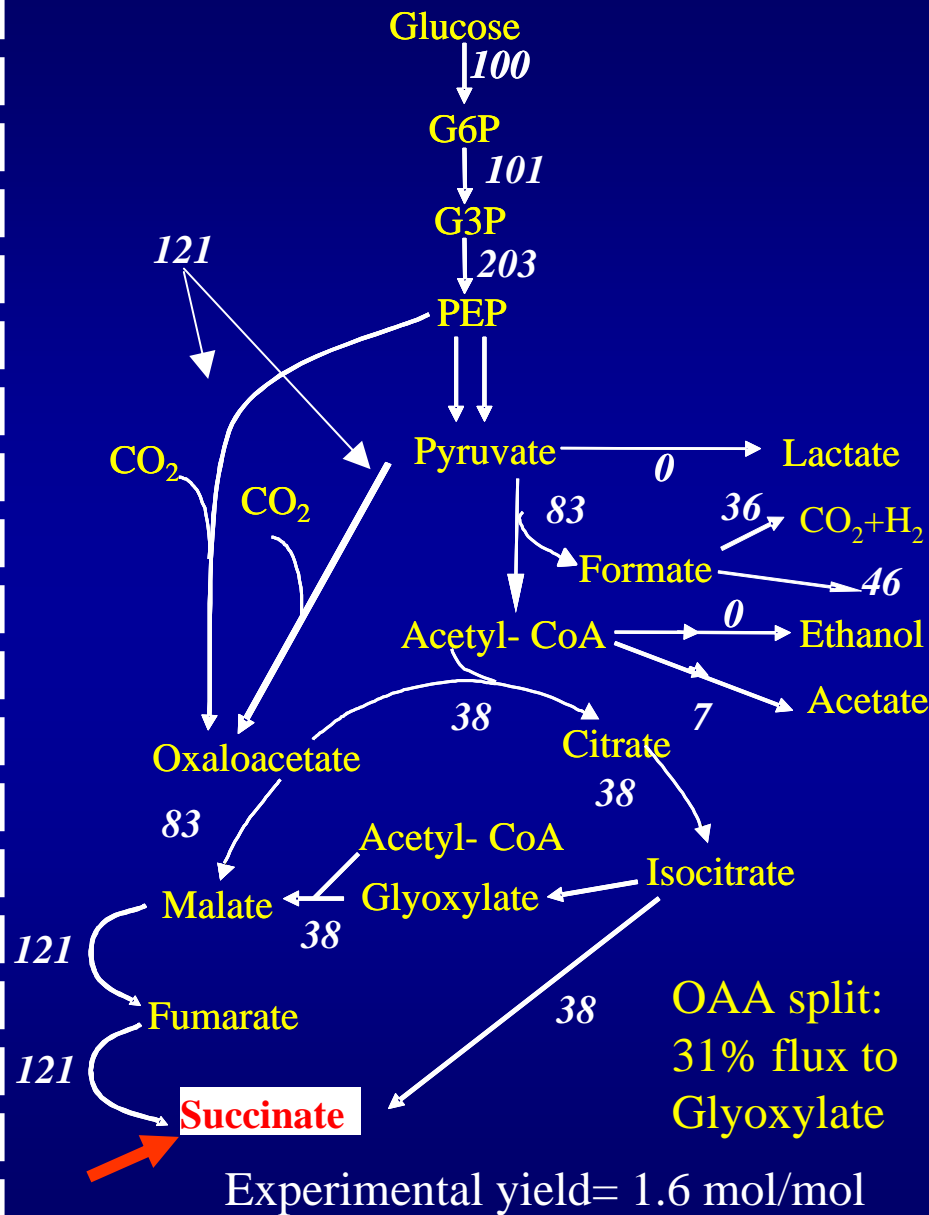
89% vs  
69%



PATHWAY DESIGN  
THEORETICAL OPTIMIZATION



PATHWAY IMPLEMENTATION  
CALCULATED FLUXES FROM EXPERIMENTAL DATA



# Summary (anaerobic)

- We have successfully designed and implemented a very robust dual-route succinate production system
- This system converts glucose to succinate at fast rates and high yields with minimal by-products
- The yield\* is very close to the maximum theoretical value
- The NADH requirement is reduced relative to the sole fermentative pathway, from two moles of NADH per mole of succinate to  $\sim 1.25$  therefore maximizing succinate production

\* during production phase

# Aerobic succinate production system

# Reconstructing the TCA cycle and glyoxylate bypass

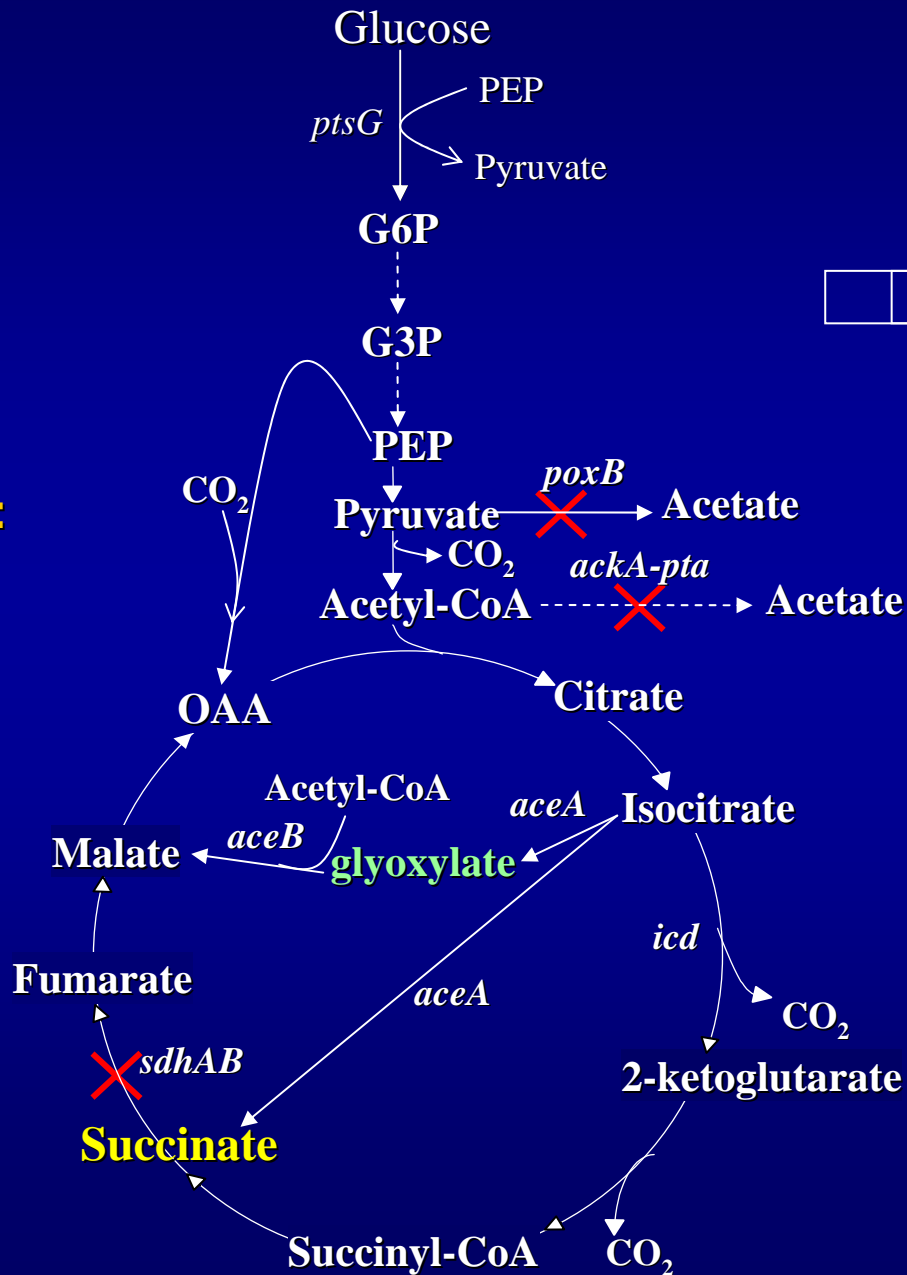
## DNA Techniques:

λ Red recombinase

P1 phage transduction

Verified by genomic PCR

**Max. theoretical yield:**  
1.0 (mol succinate/ mol glucose)



*sdhAB* - 2

*iclR* - 5

*poxB* - 6

*ackA-pta* - 7



# Two routes engineered for succinate production

## Strain HL2765k

Genes inactivated:

*sdhAB* - 2

*ackA-pta* - 7

*poxB* - 6

*iclR* - 5

## Strain HL27659k

Genes inactivated:

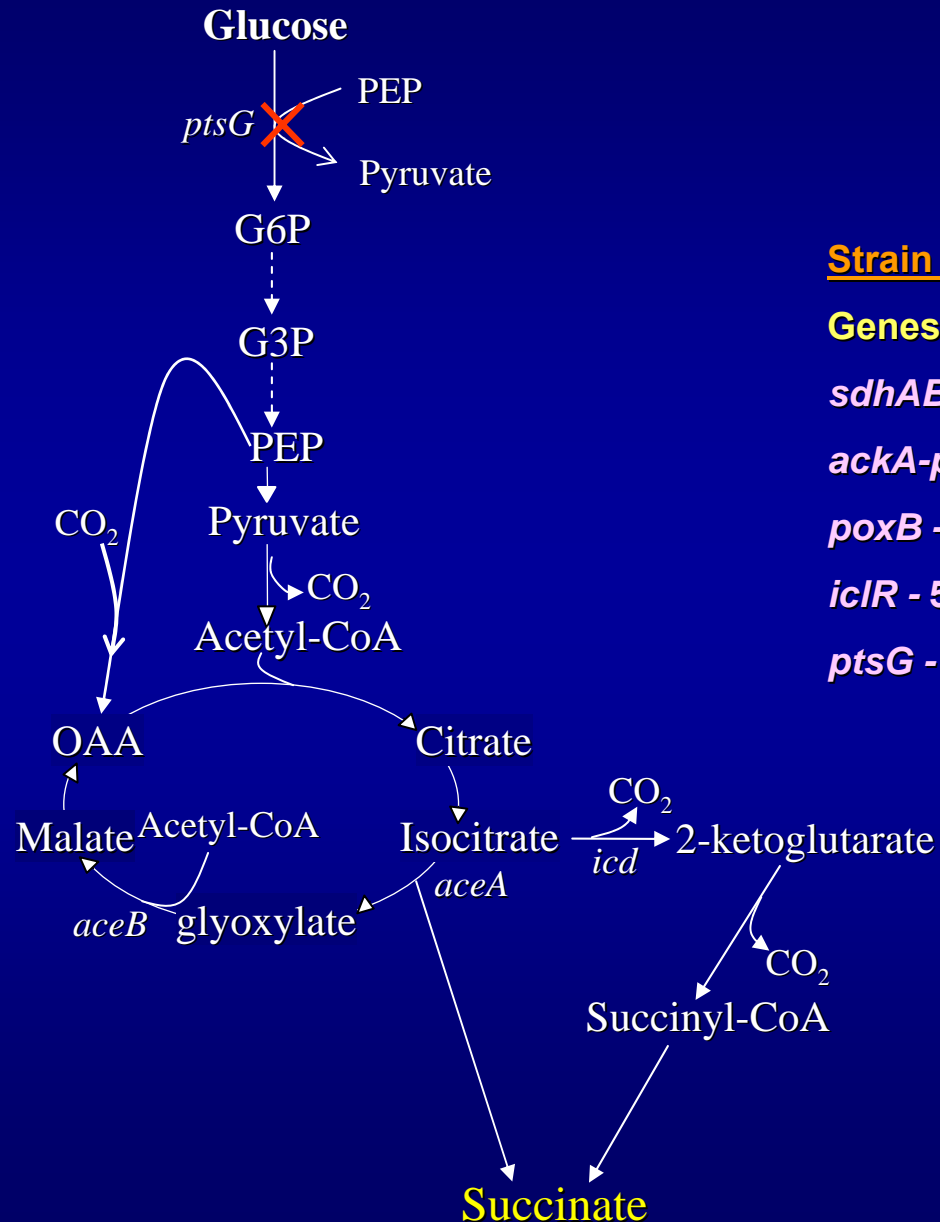
*sdhAB* - 2

*ackA-pta* - 7

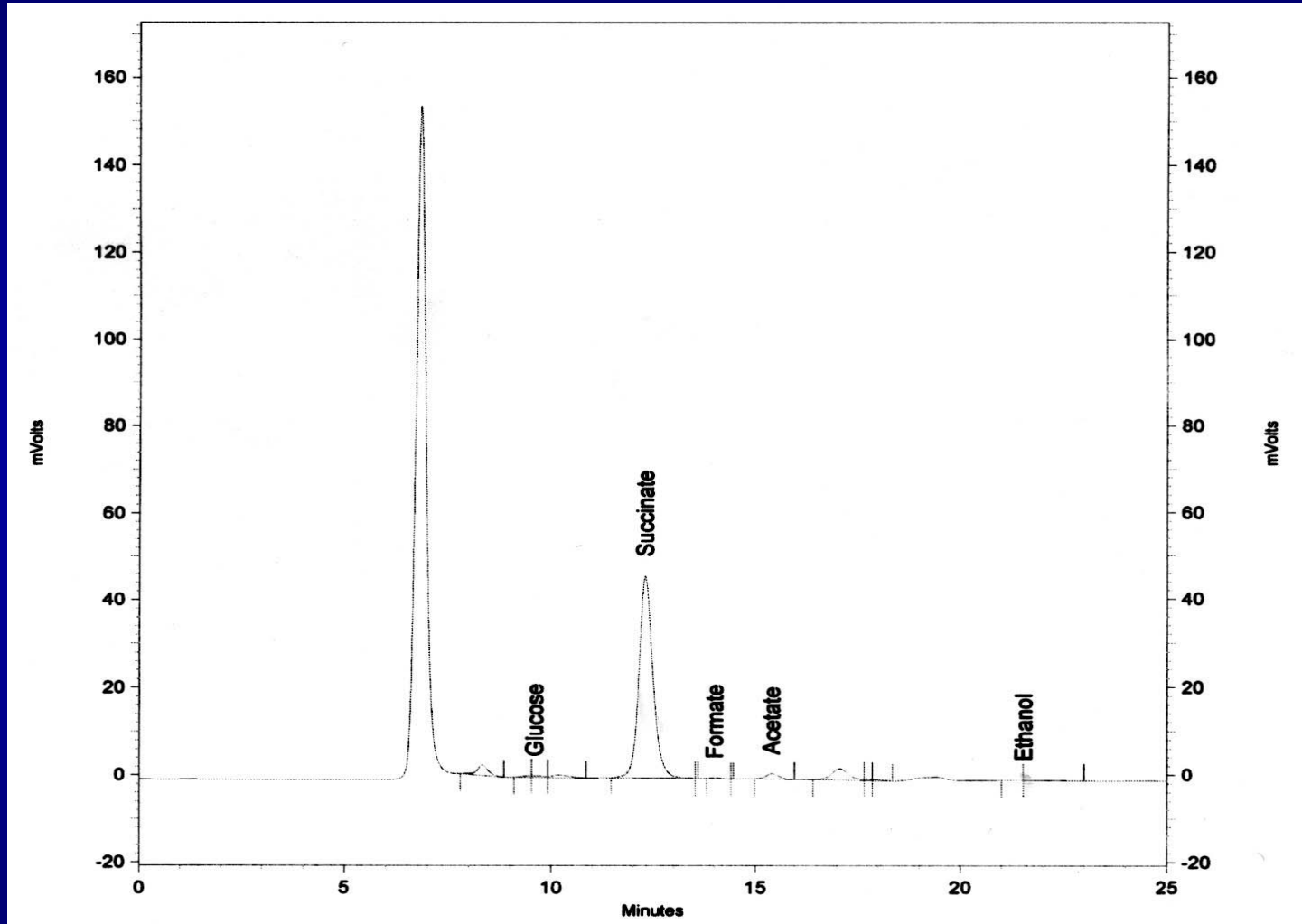
*poxB* - 6

*iclR* - 5

*ptsG* - 9

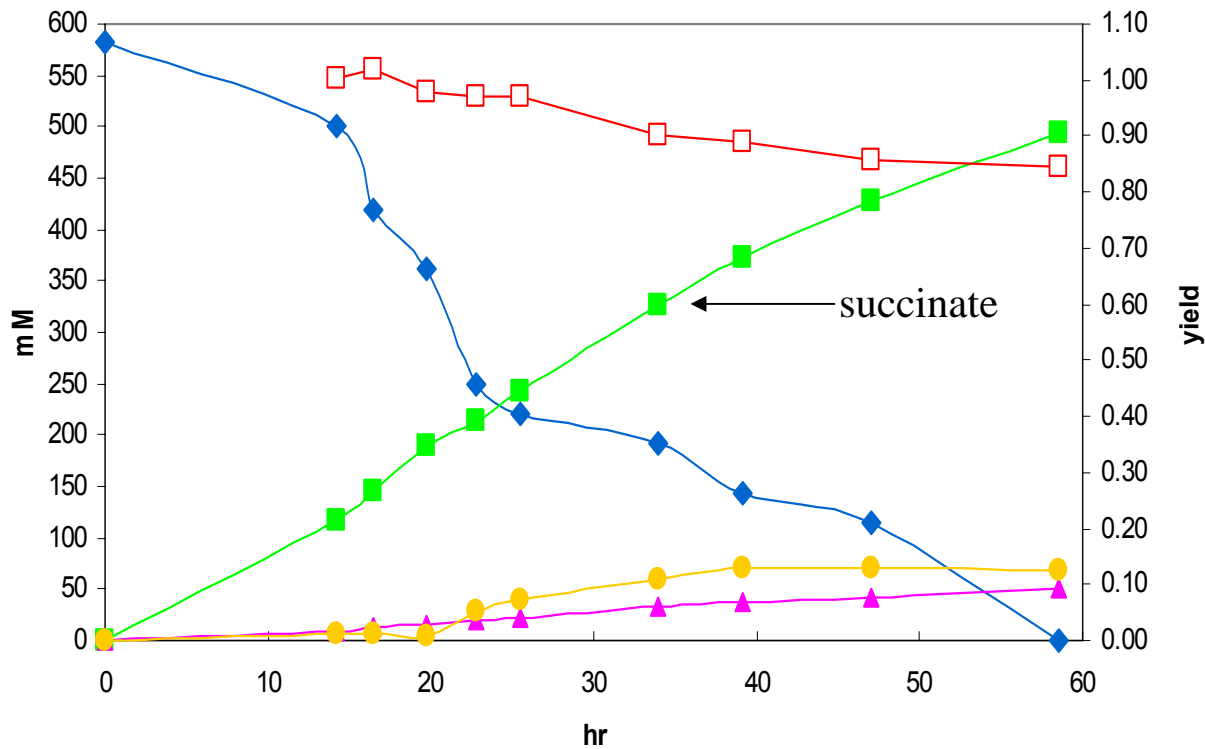


# HPLC metabolite output for strain HL27659k(pKK313)



**Strain HL27659k(pKK313) is the aerobic succinate production system**

# Fed batch culture of strain HL27659k(pKK313)



- **58.25 g/l (493.63 mM) succinate produced in 59 hrs**
- **Average succinate yield was  $0.94 \pm 0.07$  mol/mol glucose**
- **Average productivity was  $1.08 \pm 0.06$  g/l-hr**
- **Average specific productivity was  $89.77 \pm 3.40$  mg/g-hr.**

# Summary (aerobic)

- We have successfully designed and implemented a very robust dual-route aerobic succinate production system
- This system converts glucose to succinate at fast rates and high yields with minimal by-products
- The synthesis of succinate through these two pathways does not require any NADH

# Hybrid succinate production systems

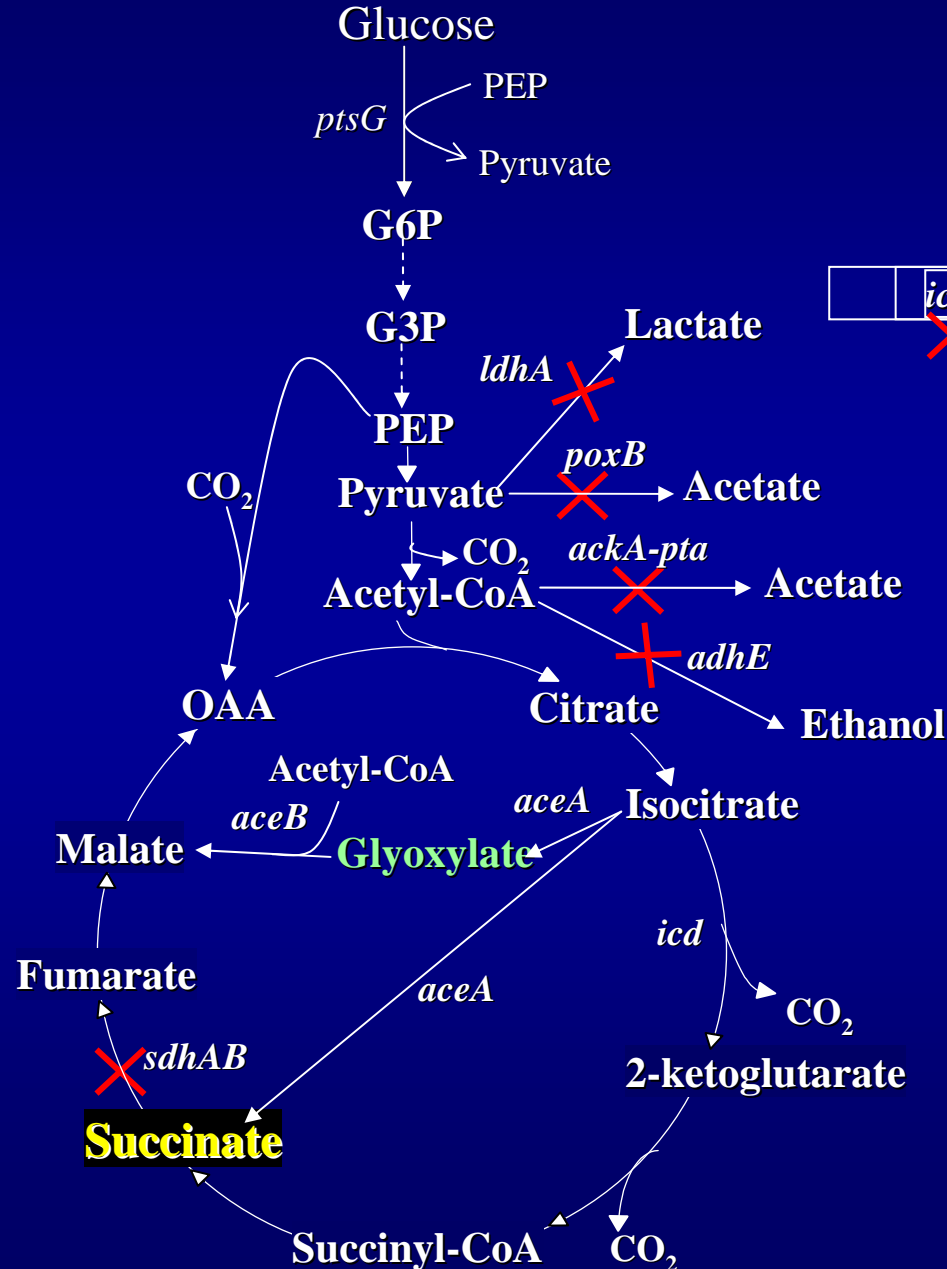
# Construction of a hybrid succinate production system

## DNA Techniques:

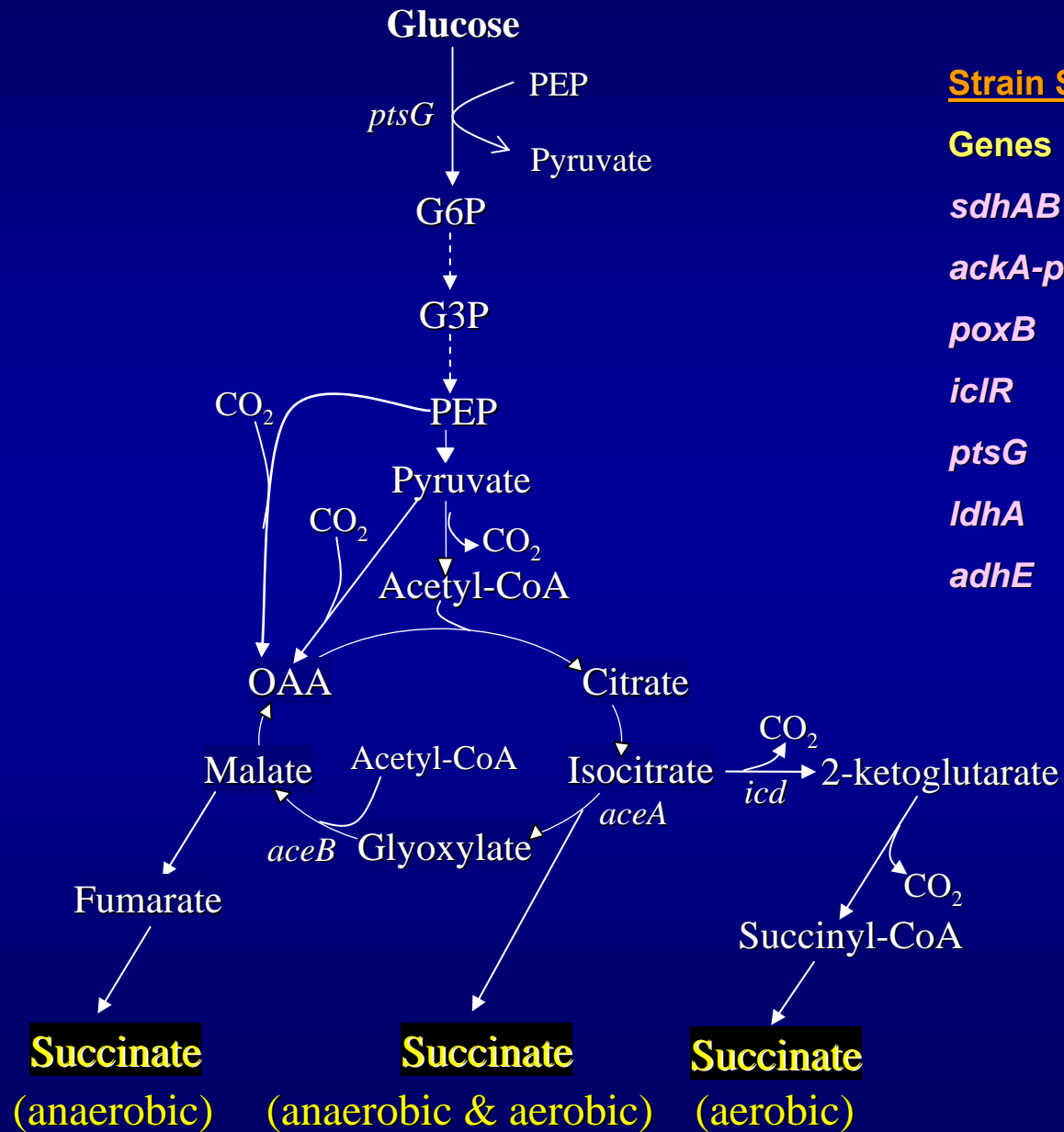
λ Red recombinase

P1 phage transduction

Verified by genomic PCR



# Three routes engineered for succinate production



# Overall Summary

- **We have developed:**
  - **an efficient aerobic succinate production system with a molar yield of close to 1**
  - **a high yield anaerobic succinate production system with a molar yield of close to 1.6**
  - **A hybrid system that is capable of producing succinate under aerobic and anaerobic conditions**
- **Same technology can be used to produce other C-4 compounds, such as fumarate and malate**



# **Acknowledgments**

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**Graduate Students:** Ailen M. Sanchez  
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